



Definition of Electrosubmersible pump (ESP) design and selection workflow

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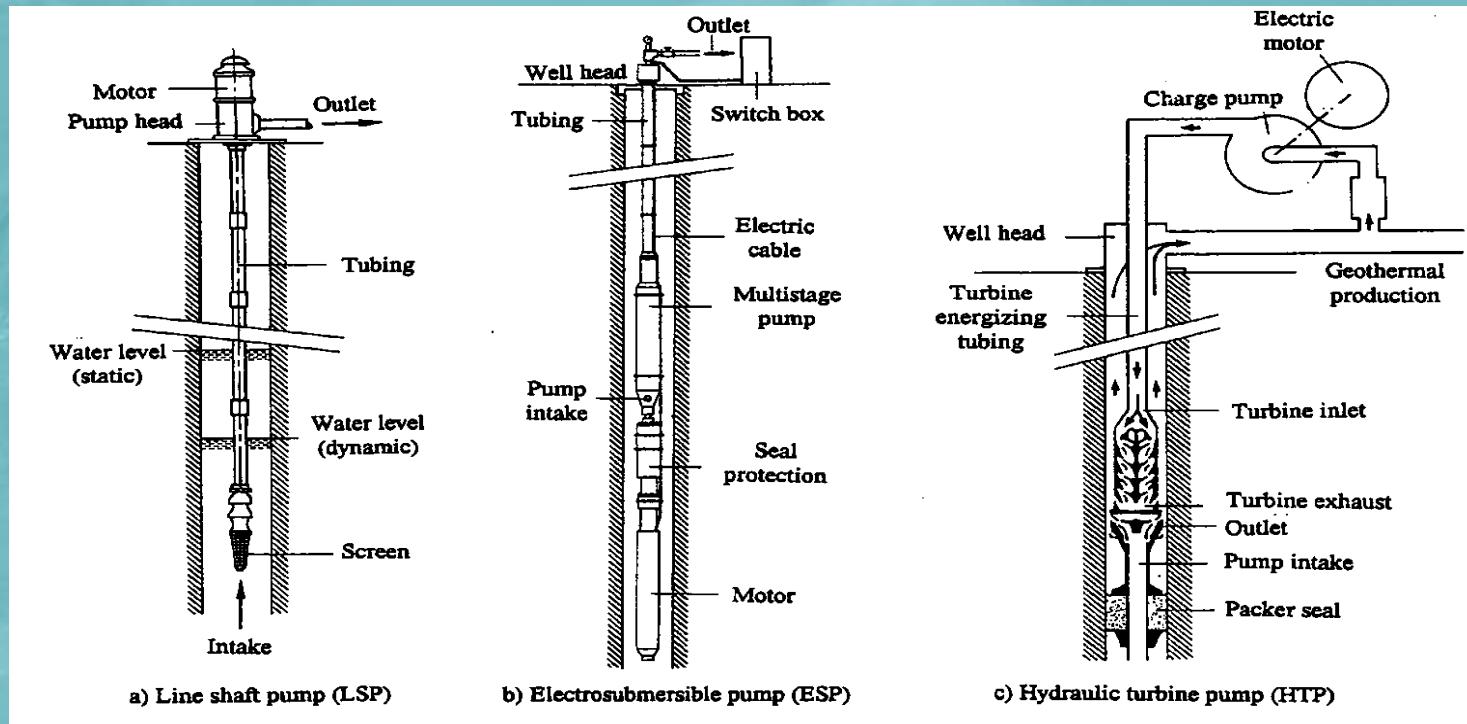
1. Introduction- work scope
2. Background
3. Survey of ESPs in Europe
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5. Recommendations

1. Introduction

Work scope

1. Review of ESP performance in Europe
2. Optimizing pump (life, COP) performance
3. Securing ESP reliability

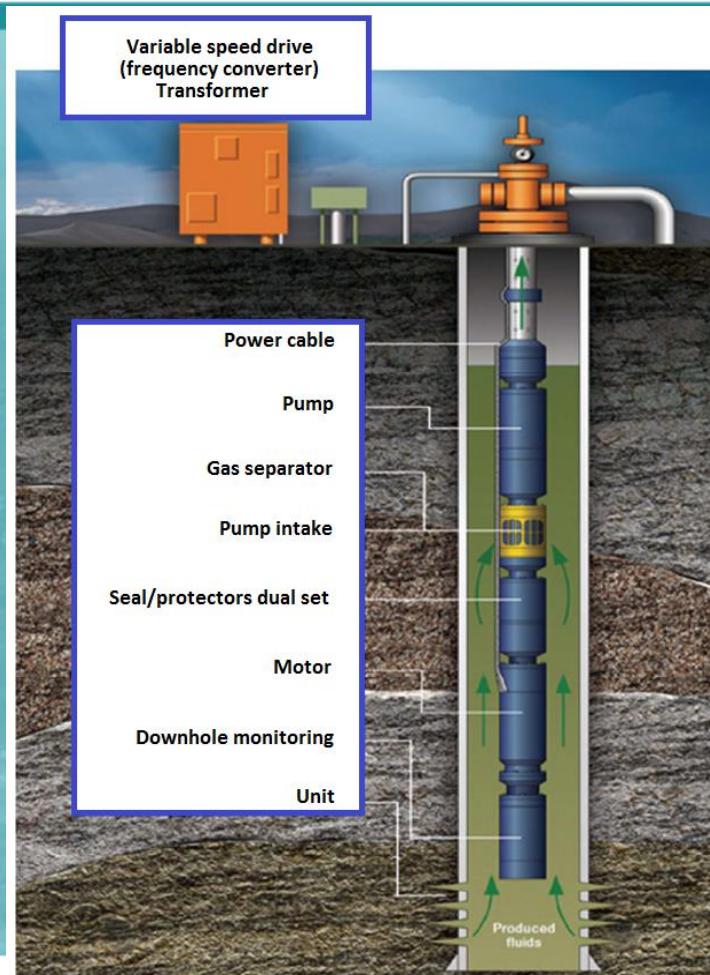
2. Background: pump types



2. Background: comparison

PUMP TYPE	Efficiency	Depth	Temperature	Suppliers	Pros	Cons
Lineshaft pumps	~ 50 %	limited to 500-600 mbgl	150-200 °C	Limied availability	Motor, seals, bearings are at surface	Long installation time. Requires perfect alignment
Electro submersible pumps	55-60%	~ 300 to ~ 1700 m	Mostly < 120 °C	Highly competitive market	Short installation time, easy handling	Less accessible motor, seals and bearings
Hydraulic turbine pumps	40%	~ 500 m		Limited availability	No electrical parts in well	Limited experience Anchoring damages well casing

2. Background: ESP construction



2. Background: ESP design

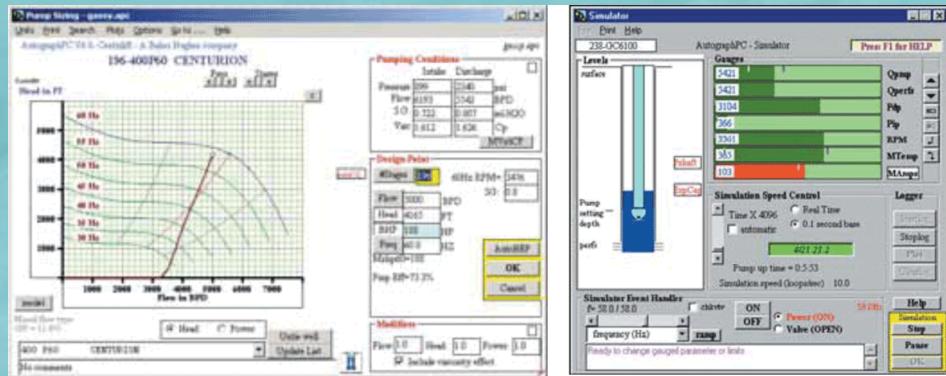
Derive Well inflow curve

Calculate required power rating

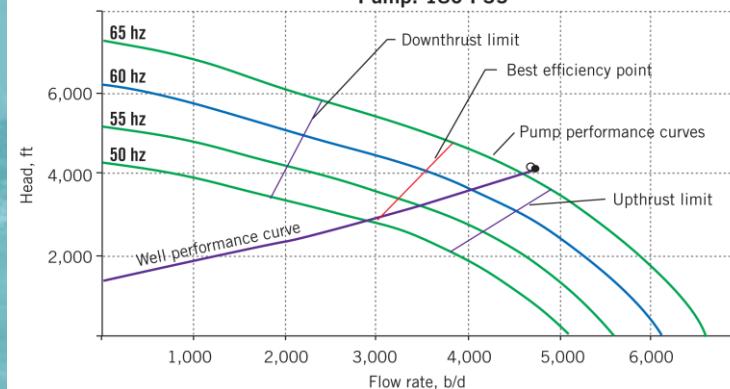
Select pump and pump set depth

Select motor, seals and power cable

Select transformer and variable speed driver



VARIABLE-SPEED PUMP PERFORMANCE



2. Background: efficiencies

$$\eta_{total} = \eta_{pump} \eta_{motor} \eta_{eleccable} \eta_{transformer} \eta_{freq}$$

η_{pump}	pump efficiency	$\sim 70\%$
η_{motor}	motor efficiency,	$\sim 90\%$
η_{cable}	electrical cable efficiency	$\sim 97\%$
$\eta_{transformer}$	efficiency of transformer	$\sim 99\%$
$\eta_{frequency}$	efficiency of frequency converter	$\sim 94\%$
η_{total}	overall efficiency	$\sim 55\%$

3. Survey in Europe: Overview

Country	Area	Description
France	Paris Basin	<ul style="list-style-type: none"> • LSP, ESP, HTP s have been operated → Currently only ESPs are operational • Highly corrosive water → control with inhibitors improves ESP life to 5 years
Germany	Molasse Basin (Munich)	<ul style="list-style-type: none"> • High temperature wells, forbidden to inject inhibitors • Results in short lifetimes of ESP (< 1 year)
	Upper Rhine Graben	<ul style="list-style-type: none"> • High temperature wells, forbidden to inject inhibitors • LSP lifetime ~ 3 years
Iceland		<ul style="list-style-type: none"> • Lifetime of 4 years for ESPs

3. Survey in Europe: Trends

Summary and outlook:

- The use of in hole corrosion and scaling inhibition increases the pump life.
- The performance of lineshaft pumps is strongly site specific, and in most instances limited to medium enthalpy producer wells, within the 150°C to 200°C range,
- ESPs are leading the low enthalpy geothermal sector (70- 120°C) range with 4 to 5 year pump life objective.
- ESPs could step into the medium enthalpy slot manufacturing majors.

4. Survey in the Netherlands

- Questionnaire sent to operators, 8 out of 13 responded
- Overall, ESPs operate at
 - Flow rates between 100-300 m³/h,
 - At temperatures between 80 and 100 °C.
- Baker Hughes ESPs have been installed in almost all wells, predicts a lifetime of ~ 5 years.
- Some ESPs operate at edge of specified range of manufacturer
 - may lower lifetime
 - results in lower efficiency
- With available data not possible to assess ESP efficiency

4. Survey in the Netherlands: Impact of lower efficiency

Example:

Power of ESP pump is 400 kW
8500 operating hours

Assume efficiency of 35% instead of 55%.
Assume electricity price of € 0,06/kWh

Avoidable electricity costs of

$$= (55-35)\% * 400 * 0,06 = € 40.800,- \text{ on a yearly basis.}$$

Table 6: ESP OPEX

(*) yearly provision assuming a four year life



4. Survey in the Netherlands: OPEX and CAPEX costs

ITEM	DESCRIPTION	CAPEX COST (k€)	
		Min	Max
1	Pump		
2	Upper Seal		
3	Lower Seal		
4	Motor		
5	Cable		
6	Monitoring/Control Unit		
7	Shipment		
8	Field service (ESP operator)		
9	ESP RIH crew		
	TOTAL	180	300

ITEM	DESCRIPTION	OPEX COST (k€/yr)	
		Min	Max
1	Monitoring/Light maintenance	10	10
2	ESP replacement (*)	35	60
3	POOH damaged ESP (*)	5	7
4	RIH new ESP (*)	7.5	9
5	Contingencies	6	9
	TOTAL	63.5	95

5. Recommendations

ESP design:

- Utilize design guidelines on expected reservoir performance. Record well deliverability and fine tune the design
- Account for potential degradation of well and reservoir performance
- Utilize tandem (two seal) protect in ESP

5. Recommendations

ESP maintenance:

- Record periodically performance of ESP (working point, efficiencies, reactive current, harmonic distortion,...)
- Utilize sound O&M protocols
- ESPs are designed for continuous operation → Limit number of starts/stops
- Utilize chemical inhibition to protect ESP
- Spare parts on stock for fast duty cycles

